# **RESEARCH ARTICLE**

**Open Access** 



# Synthesis of bimannich base with thiazole and its corrosion inhibition effect on H<sub>2</sub>S and CO<sub>2</sub> at high temperature

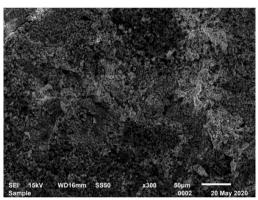
Li Zhuoke<sup>1,2,3\*</sup>, Cao Jun<sup>1,2,3</sup>, Mao Ting<sup>1,2,3</sup> and Ni Dan<sup>4</sup>

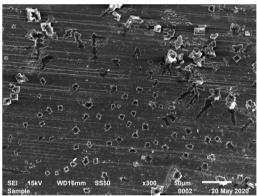
#### **Abstract**

A bimannich-based TZBM containing a thiazole ring was obtained by synthesis of mannich bases. TZBM featured a stable structure at 260 °C, and corrosion inhibition effect on carbon steel in a gas—liquid environment with  $Cl^- + H_2S + CO_2$  at 180 °C. By analyzing the weight loss of steel exposed to different TZBM concentrations, the coverages of the inhibitor adsorbed on the surfaces were determined, and the results conformed to Langmuir isotherm model. Furthermore, the negative Gibbs free energy indicated that the adsorption was a spontaneous process.

Keywords: Thiazole, Bimannich base, Corrosion inhibitor, High temperature resistance

# **Graphical Abstract**





# Introduction

The sour gas and sour water are highly corrosive to the metal materials when passing through the pipelines. For example, as to the pipelines of sour gas wells, corrosion inhibitors are applied on the metal pipes to improve the gas transmission environment [1-3], ensure safe

\*Correspondence: 824613768@qq.com

production and extend the service life of metal pipes. The research field of corrosion inhibitors used in the oil–gas gathering and transmission system is mature because of the mild conditions [4–7]. However, as for the corrosion inhibitors used in downhole, due to the more complex conditions and higher temperatures in the deeper places, the effect of the existing inhibitors is reduced.

The most popular corrosion inhibitor for H<sub>2</sub>S and CO<sub>2</sub> is imidazoline corrosion inhibitor, which is widely used in oil and gas fields, especially in pipelines, and is proven



© The Author(s) 2021. **Open Access** This article is licensed under a Creative Commons Attribution 4.0 International License, which permits use, sharing, adaptation, distribution and reproduction in any medium or format, as long as you give appropriate credit to the original author(s) and the source, provide a link to the Creative Commons licence, and indicate if changes were made. The images or other third party material in this article are included in the article's Creative Commons licence, unless indicated otherwise in a credit line to the material. If material is not included in the article's Creative Commons licence and you rintended use is not permitted by statutory regulation or exceeds the permitted use, you will need to obtain permission directly from the copyright holder. To view a copy of this licence, visit http://creativeccommons.org/licenses/by/4.0/. The Creative Commons Public Domain Dedication waiver (http://creativeccommons.org/publicdomain/zero/1.0/) applies to the data made available in this article, unless otherwise stated in a credit line to the data.

<sup>&</sup>lt;sup>1</sup> Southwest Oil and Gas Field Branch, Research Institute of Natural Gas Technology, Petrochina Ltd, Chengdu, Sichuan, China Full list of author information is available at the end of the article

Zhuoke et al. BMC Chemistry (2021) 15:59 Page 2 of 8

to be effective. The main method to get imidazoline corrosion inhibitors is the two-step dehydration of polyvinyl polyamines and long-chain acids. The first step of dehydration is carried out at  $140-160\,^{\circ}\text{C}$ , and the second step at  $200-230\,^{\circ}\text{C}$  [8–14]. Reaction conditions are very important. In addition, organic compounds containing hetero-atoms such as N, O and S are also proven corrosion inhibitors for metals and alloys [15–20]. The Mannich base is usually used as the corrosion inhibitor for well acidizing treatments, requiring only one step with a reaction temperature of  $60-80\,^{\circ}\text{C}$  and mild conditions [21–26]; however, it is seldom used for  $\text{H}_2\text{S}$  and  $\text{CO}_2$  environment. Studies have shown that the synthetic bis-Mannich base outperforms the Mannich base.

In this paper, a bis-Mannich base with thiazole synthesized in the laboratory turned out to be an effective corrosion inhibitor for the steel exposed to corrosive liquid containing  $Cl^- + H_2S + CO_2$ , so this compound is an option for the corrosion protection for the  $H_2S$  and  $CO_2$  environment.

# **Experiment**

# Substances

2-Acetylthiazole(AR), Benzaldehyde(AR), Tetraethylenepentamine(AR), Hydrochloric Acid (AR), Absolute Ethanol (AR), Petroleum Ether (AR), NaCl (AR), Carbon dioxide (99.999%), Nitrogen (99.999%), Hydrogen sulfide (99.99%).

# **Synthesis**

One-pot synthesis was implemented as follows to get bimannich-based TZBM. First, benzaldehyde was added to the ethanol (solvent) in the three-neck flask. Tetraethylenepentamine was then slowly added, followed by 2-acetylthiazole. The molar ratio of the three solutes was 2:2:1. Concentrated hydrochloric acid was slowly added till the pH value is  $4 \sim 5$ . The solution was heated till the temperature reaches 80 °C for condensation and reflux. 6 h later, a reddish-brown liquid was obtained, and crude TZBM could be obtained after distillation under reduced pressure. Finally, it was recrystallized with absolute ethanol 2–3 times to obtain a purer product. Reaction equation is illustrated in Scheme 1.

#### Thermogravimetric analysis

The thermogravimetric analysis (TGA) of TZBM was carried out in the nitrogen atmosphere using Mettler Dsc823 supplied by METTLER TOLEDO. The starting temperature was 40 °C, and the heating rate was 10 °C/min.

# **Gravimetric analysis**

The size of the specimens for weight loss measurements was  $30 \text{ mm} \times 15 \text{ mm} \times 3 \text{ mm}$ . Surface finishing was conducted with emery paper (400-1000 Grit).

Atmospheric pressure experiment: 1 Nitrogen was added for 8 h, to remove the oxygen in NaCl solution (5.0L, 5.0%). The deoxygenated NaCl solution was halved in two containers.  $2CO_2$  was gently added to the deoxygenated NaCl solution (2.5L, 5.0%) for 8 h to get the CO<sub>2</sub>-saturated solution. At the same time, H<sub>2</sub>S was gently added to the deoxygenated NaCl solution (2.5L, 5.0%) for 8 h to get the H<sub>2</sub>S-saturated solution. 3The CO<sub>2</sub>-saturated solution and the H<sub>2</sub>S-saturated solution were mixed at 1:1 to get the corrosion solution. **(4)**Two specimens were immersed into the corrosion solutions with/without TZBM at different concentrations in oil bath at 80 °C, and oxygen was removed by nitrogen. ⑤72 h later, the specimens were taken out, rinsed with distilled water, washed with the membrane-removing acid solution, alcohol, and petroleum ether, dried, and weighed using an analytical balance having a readability down to 0.01 mg.

High-temperature and high-pressure test: 650 mL 5.0% NaCl solution and a calculated amount of corrosion inhibitor were added into the autoclaves, and two specimens were hung into the autoclaves and immersed in the liquid. Nitrogen was blown in for 6 h, to remove oxygen. The autoclaves were sealed. After 2.0 MPa  $\rm CO_2$  and 1.0 MPa  $\rm H_2S$  were added in the autoclaves, nitrogen was added till the total pressure is 10 MPa. Two specimens were immersed into the corrosion solutions with/without TZBM at different concentrations at 180 °C. 72 h later, the specimens were taken out, rinsed with distilled water, washed with the membrane-removing acid solution, alcohol, and petroleum ether, dried, and weighed using an analytical balance having a readability down to 0.01 mg.

Zhuoke et al. BMC Chemistry (2021) 15:59 Page 3 of 8

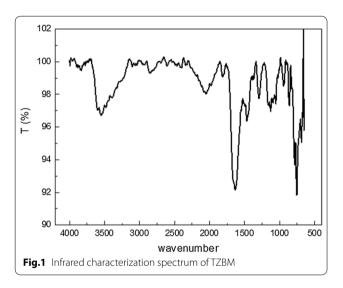
# Observation of corrosion morphology

The surfaces of the specimens undergoing the high-temperature and high-pressure test without being rinsed were observed with a scanning electron microscope (JSM-6510), which could help analyze the corrosion inhibition effect of TZBM on the specimens in gas–liquid environment exposed to  $Cl^- + H_2S + CO_2$ . And EDS test by the scanning electron microscope was used for quantitative analysis of element content, to determine the formation of corrosion products.

# **Results and discussion**

# Structure characterization

Figure 1 shows the infrared spectroscopy of TZBM. The graph presents a single peak at 3542 cm<sup>-1</sup>, which is the

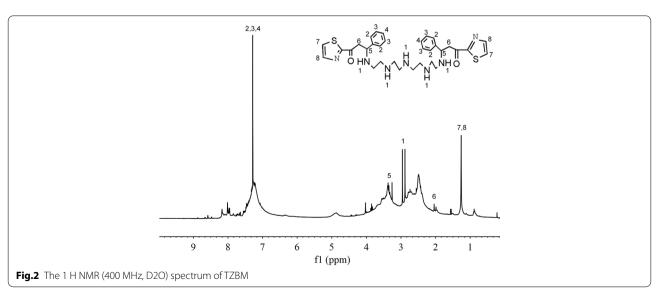


characteristic peak of the stretching vibration of the secondary amine N–H bond. The stretching vibration peak of the methylene C-H bond appears at 2862 cm<sup>-1</sup>, and the carbonyl group becomes connected to the heterocyclic ring at 1646 cm<sup>-1</sup>. The C=N double bond in the thiazole has the stretching vibration peak at 1461 cm<sup>-1</sup>, and fingerprint regions (745 cm<sup>-1</sup> and 675 cm<sup>-1</sup> ranges) are characteristic peaks of CH deformation vibrations monosubstituted by benzene ring. Meanwhile, there is no obvious narrow double peak at 3500 ~3400 cm<sup>-1</sup>, indicating that there is no functional group of primary amines; there is no strong peak at 1720 cm<sup>-1</sup>, indicating that there is no C=O double bond of aldehyde. It shows that the reaction is completed and the target product is successfully synthesized.

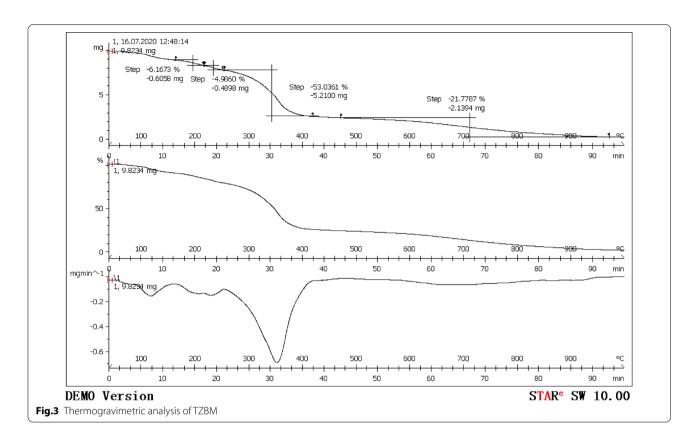
The  $^1$  H NMR in Fig. 2 further verifies the synthesis of TZBM. The 2.88 ppm point shows the chemical shifts of protons of polyamines marked as 1. The peak of the chemical shift of protons of -CH- of benzene backbones is found at 7.27 ppm (marked as 2, 3 and 4). The peak at 3.28 ppm (marked as 5) is the peak of the chemical shift of protons of the -CH- bonded with N atom of the polyamines. 2.06 ppm shows the chemical shifts of the protons of the  $-CH_2-$  bonded with C=O marked as 6. The peak of the chemical shift of protons of Thiazole rings is found at 2.25 ppm (marked as 7 and 8). The molecular structure of synthesized AHAPAM obtained from  $^1$  H NMR spectrum is consistent with that obtained from the FTIR spectrum.

# Thermogravimetric analysis

Figure 3 shows that the initial weight of the tested TZBM sample is 9.8234 mg. As the temperature gradually increases, the weight of TZBM firstly is unchanged



Zhuoke et al. BMC Chemistry (2021) 15:59 Page 4 of 8



and then drops sharply and finally is unchanged again. In the temperature range of 260–400 °C, the weight of TZBM drops sharply by 53%. The rate of weight loss first increases and then decreases, and reaches a maximum value of about 0.8 mg/min at about 360 °C. These indicate that the chemical structure of TZBM is stable at 260 °C, and that the structure becomes unstable and the chemical bond breaks when the temperature exceeds 260 °C. Therefore, TZBM is of excellent temperature resistance when used in the natural gas gathering pipelines and downhole.

# Weight loss measurements

Table 1 shows the inhibitor efficiency and corrosion rates obtained from weight loss measurements with different concentrations of the inhibitor in the prepared corrosion solution at  $80\pm0.1$  °C. With the weight loss calculated, the inhibitor efficiency  $\eta$  is calculated using the following equation:

$$\eta = (R0 - R)/R0 \times 100\% \tag{1}$$

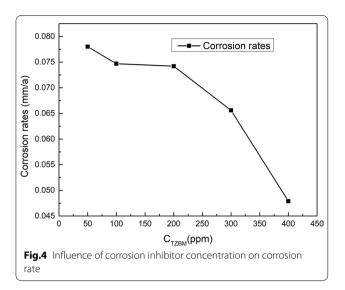
where R and R<sub>0</sub> are rates of corrosion (mm/a) with/without inhibitor.

**Table 1** Inhibition efficiency for various concentrations of TZBM for the corrosion of steel in the prepared corrosion solution obtained from weight loss measurements

C <sub>TZBM</sub> (ppm)	Corrosion rates (mm/a)	Inhibitor effificiency (%)	
Blank	2.1897	_	
50	0.0780	96.44	
100	0.0747	96.58	
200	0.0742	96.61	
300	0.0656	97.0	
400	0.0479	97.81	

Figure 4 shows that corrosion rate decreases with increase in TZBM concentration. In the concentration range of 50--200 ppm, the corrosion rate reduces slowly. It means that if the amount of corrosion inhibitor is small, the specimen surface cannot be fully covered. When the concentration of the corrosion inhibitor exceeds 300 ppm, the corrosion rate is significantly reduced. At 400 ppm, the corrosion rate is only 0.0479 mm/a, indicating that when the corrosion

Zhuoke et al. BMC Chemistry (2021) 15:59 Page 5 of 8



inhibitor fully covers the surface of the specimen, it can effectively block the corrosive medium and protect the steel.

# Adsorption isotherm

To understand the mechanism of corrosion inhibition, it is necessary to know the adsorption behavior of the organic adsorbate on the metal surface.

The main assumptions of the Langmuir adsorption model proposed by Irving Langmuir are the following: ①The adsorption and desorption on the surface are reversible and reach a dynamic equilibrium; ②The surface of the adsorbent still has residual forces for attraction. The adsorption capacity is the same; ③The adsorption occurs at the single-molecule site, and the maximum surface coverage  $\theta$  is 1; ④The adsorbed medium have no influence on each other. Therefore, the Langmuir isotherm equation can be expressed as Eq. 2 [27–29].

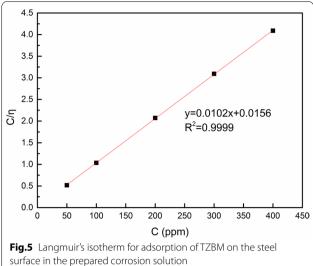
$$\theta = K\alpha/(1+K\alpha) \tag{2}$$

where,  $\theta$  is the surface coverage, K is the thermodynamic equilibrium constant of adsorption, and a is the activity of corrosion inhibitor.

For the assumed simple-molecule adsorptive behavior of TZBM, inhibition efficiency  $\eta$  can replace surface coverage  $\theta$ . And in low concentration. The activity of corrosion inhibitor a can be replaced by the concentration C. Therefore, Eq. 3 is derived from Eq. 2.

$$C/\eta = C + 1/K \tag{3}$$

Considering the influence of other factors, we adapt Eq. 3 by multiplying a correction factor f, and Eq. 4 is as follows.



$$C/\eta = fC + f/K \tag{4}$$

According to Table 1, the surface coverage is tested to allow fitting of a suitable adsorption isotherm. The plot of  $C/\eta$  versus C (Fig. 5) yields a straight line with nearly unit slope, proving that the adsorption of the TZBM from the prepared corrosion solution on the steel obeys the Langmuir adsorption isotherm [30, 31].

The equilibrium adsorption constant K obtained from the Langmuir plot is about  $0.65 \times 10^3$  l/mol. From Van't Hoff equation (Eq. 5),  $\Delta G$  is - 19.02 kJ/mol, which indicates that TZBM is strongly adsorbed on the steel surface, and that this adsorption process is spontaneous.

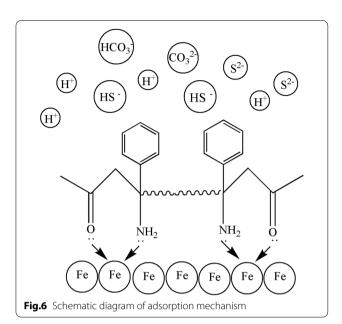
$$\Delta G = -RT \ln K \tag{5}$$

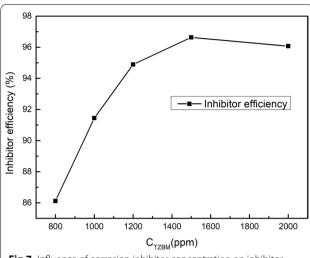
From this analysis, TZBM prevents corrosive media from passing through single molecules adsorbed on the surface of the steel. The principle of adsorption is that the N and O atoms in the molecule contain a lone pair of electrons, which can enter the hybrid orbital of the iron atom in the steel to form a coordination bond. Because of the special structure of TZBM, this coordination bond just establishes a stable six-membered ring structure, and each molecule can form two adsorption points, as shown in Fig. 6, so that TZBM is more firmly adsorbed on the surface of steel, which improves its high temperature resistance.

# High-temperature and high-pressure test

Since temperature has a great influence on the corrosion rate, to ensure the corrosion inhibition effect of TZBM, the concentration of TZBM was increased to 1500 ppm in the high-temperature and high-pressure test. Table 2 shows the results of high-temperature

Zhuoke et al. BMC Chemistry (2021) 15:59 Page 6 of 8



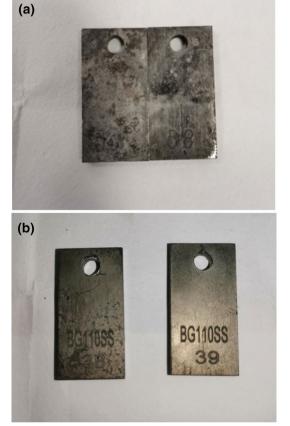


**Fig.7** Influence of corrosion inhibitor concentration on inhibitor efficiency in the high-temperature and high-pressure test

**Table 2** The results of high temperature and high pressure test for corrosion inhibition performance of TZBM

C <sub>TZBM</sub> (ppm)	Corrosion rates (mm/a)	Inhibitor efficiency (%)	
Blank	1.6156	=	
800	0.2242	86.12	
1000	0.1382	91.44	
1200	0.0826	94.89	
1500	0.0544	96.63	
2000	0.0635	96.07	

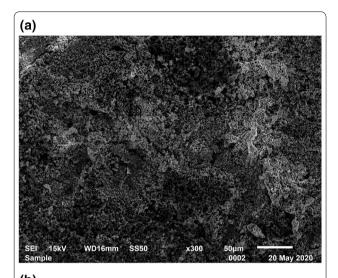
and high-pressure test for corrosion inhibition performance of TZBM at different concentration. The trends of corrosion at different concentrations is shown in Fig. 7. As the concentration increases, the corrosion inhibition efficiency gradually increases until the concentration is 1500 ppm. Because the molecular movement is violent at high temperature, it is more difficult for the corrosion inhibitor to be adsorbed on the surface of the steel. Adding more corrosion inhibitor to the solution will help increase the amount of corrosion inhibitor adsorbed on the surface of the steel to increase the corrosion inhibition efficiency. And when the corrosion inhibitor exceeds a certain concentration, the steel surface cannot absorb more corrosion inhibitor, therefor the corrosion inhibition efficiency will not increase.

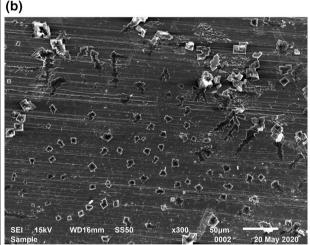


**Fig.8** a The photo of the appearance of after-cleaning specimens without inhibitor; b The photo of the appearance of after-cleaning specimens with inhibitor TZBM

Zhuoke et al. BMC Chemistry (2021) 15:59 Page 7 of 8

Figure 8 is the photo of the appearance of after-cleaning specimens with and without inhibitor, respectively. The high-temperature and high-pressure test proves that TZBM has good corrosion inhibition performance at high temperature.





**Fig.9** a Corrosion morphology of the surface of the specimen which from the test without inhibitor; **b** Corrosion morphology of the surface of the specimen which from the test with 1500 ppm inhibitor

# Corrosion morphology observation

Figure 9 shows the micro corrosion morphology of the specimens after the high-temperature and high-pressure test without being rinsed. There are large quantities of overlapping loose structures on the surface of the specimen from the test without inhibitor TZBM. The overlapping loose structures should be the corrosion products of steel. Differently, some crystalline objects can be observed on a flat surface of the specimen from the test with 1500 ppm inhibitor TZBM. Those crystalline objects should be NaCl precipitating from the corrosion solution.

Table 3 shows the distinguish of corrosion products on the surface in the corrosion solutions with/without TZBM. From the EDS test, the surface of the specimen from blank test has 28.95% atom S, but with TZBM there is only 4.43%. It means TZBM significantly reduced the production of iron-sulfur compounds.

Through the observation of corrosion morphology, the result of adsorption behavior research is confirmed. TZBM can indeed adsorb stably on the surface of steel to block corrosive medium at high temperature.

#### **Conclusions**

- The bis-Mannich-based TZBM containing thiazole structure is stable at the temperature below 260°C.
- TZBM inhibits the corrosion of steel in a gas-liquid environment containing Cl-+H<sub>2</sub>S+CO<sub>2</sub>.
- According to the weight loss experiment, the higher the concentration of inhibitor, the higher the inhibition efficiency.
- The adsorbed inhibitor molecules on the steel surface blocks corrosive medium and therefore inhibits corrosion. Adsorption of the inhibitor conforms to the Langmuir isotherm model.
- Enough TZBM forms a stable protective layer on the surface of the steel in the corrosive solution at 180 °C, and the corrosion rate of the steel is lower than 0.076 mm/a. This shows that TZBM is an excellent corrosion inhibitor for high-temperature environment.

Table 3 The percentage of atoms on the surface of the specimen from the test without/with 1500 ppm inhibitor

Element	С	0	Na	S	Cr	Fe
The percentage of atoms (blank)	14.09	18.63	2.50	28.95	0.22	35.61
The percentage of atoms (1500 ppm TZBM)	12.55	19.39	5.72	4.43	0.85	55.87

Zhuoke et al. BMC Chemistry (2021) 15:59 Page 8 of 8

#### Abbreviation

TZBM: The synthetic bimannich-based containing a thiazole ring in this study.

#### Acknowledgements

We are pleased to acknowledge the financial support provided by Research Projects 20190303-18 and 20190305-03 of Southwest Oil and Gas Field Branch, Petrochina Ltd.

# Authors' contributions

ZL contributed to the conception of the study. JC and TM performed the experiment. DN contributed to analysis and manuscript preparation. All authors read and approved the final manuscript.

#### Funding

This research was supported by Research Projects 20190303-18 and 20190305-03 of Southwest Oil and Gas Field Branch, Petrochina Ltd.

#### Availability of data and materials

All data generated or analyzed during this study are included in this published article.

#### **Declarations**

# Ethics approval and consent to participate

Not applicable.

#### Consent for publication

Informed consent for publication was obtained from all participants.

#### Competing interests

The authors declare no competing interests.

#### **Author details**

<sup>1</sup> Southwest Oil and Gas Field Branch, Research Institute of Natural Gas Technology, Petrochina Ltd, Chengdu, Sichuan, China. <sup>2</sup>National Energy High Sour Gas Reservoir Exploitation R&D Center, Chengdu, Sichuan, China. <sup>3</sup>High Sulfur Gas Exploitation Pilot Test Center of CNPC, Chengdu, Sichuan, China. <sup>4</sup>Northwest Sichuan Division, PetroChina Southwest Oil Gas Field Company, Jiangyou 621714, Sichuan, China.

# Received: 21 January 2021 Accepted: 12 October 2021 Published online: 03 November 2021

#### References

- Papavinasam S, Doiron A, Revie RW. Effect of Surface Layers on the Initiation of Internal Pitting Corrosion in Oil and Gas Pipelines. Corrosion -Houston Tx-. 2012;65(10):663–73.
- 2. Qu L. Analysis and Countermeasure on the corrosion of metal pipelines and vessels in oil fields. Petrol Plan Eng. 2000;98:7.
- Radkevych OI, Chumalo HV. Damage to the Metal of Industrial Pipelines in a Hydrogen Sulfide Environment. Mater Sci. 2003;39(4):596–600.
- Hu T, Wang Q, Tao G, Zhou Y. Status-quo of Corrosion and Anti-corrosion Technologies of Metal Pipelines. Corros Protect Petrochem Indus. 2008:3:45.
- Cho I. Exploring the Relationship Between Dimensions of Organizational Learning and Firms' Financial and Knowledge Performance in the Korean Business Context. Dissert Theses Gradworks. 2009;12:204.
- Fu L, et al. Study on corrosion and scale inhibition mechanism of polyaspartic acid grafted β-Cyclodextrin. Mater Lett. 2019;9:127276.
- Martínez D, et al. Amine type inhibitor effect on corrosion–erosion wear in oil gas pipes. Wear. 2009;267(1–4):255–8.
- 8. Akindeju MK, et al. Effectiveness of Imidazoline in Mitigating Transport Pipeline Corrosion. Struct Chem Crystallogr Commun. 2017;3:1.

- Lucio-Garcia MA, et al. A study of hydroxyethyl imidazoline as H<sub>2</sub>S corrosion inhibitor using electrochemical noise and electrochemical impedance spectroscopy. J Appl Electrochem. 2010;40(2):393–9.
- 10. Li J, et al. Cathodic Protection for Long Distance Oil & Gas Station. Natural Gas and Oil; 2016.
- Yang J, Jovancicevic V. Corrosion inhibitors for oilfield applications. WO, US20090181867 A1. 2009.
- 12. Xia L, Yugui Z. Effect of hydrophilic group on inhibition behaviour of imidazoline for CO2 corrosion of N80 in 3%NaCl solution. J Chin Soc Corros Protect. 2009;295:87–92.
- 13. Wahyuningrum D, et al. The synthesis of imidazoline derivative compounds as corrosion inhibitor towards carbon steel in 1% NaCl Solution. ITB J Sci. 2008;401(7):6432–8.
- Heydari M, Javidi M. Corrosion inhibition and adsorption behaviour of an amido-imidazoline derivative on API 5L X52 steel in CO<sub>2</sub>-saturated solution and synergistic effect of iodide ions. Corros Sci. 2012;61:148–55.
- Popova A, Christov M. Evaluation of impedance measurements on mild steel corrosion in acid media in the presence of heterocyclic compounds. Corros Sci. 2006;48(10):3208–21.
- 16. Li S, et al. Investigation on some Schiff bases as HCl corrosioninhibitors for copper. Corros Sci. 1999;41(7):1273–87.
- Ashassi-Sorkhabi H, Asghari E. Effect of hydrodynamic conditions on the inhibition performance of L-methionine as a "green" inhibitor. Electrochim Acta. 2008;54(2):162–7.
- Shokry H, et al. Corrosion inhibition of mild steel by schiff base compounds in various aqueous solutions (Part 2). Corros Sci. 1998:40(12):2173–86.
- Li X, et al. Inhibition effect of 6-benzylaminopurine on the corrosion of cold rolled steel in H2SO4 solution. Corros Sci. 2009;51(3):620–34.
- Ishtiaque A, Ahamad PB. Thermodynamic, electrochemical and quantum chemical investigation of some Schiff bases as corrosion inhibitors for mild steel in hydrochloric acid solutions. Corros Sci. 2010;523:933–42.
- Fu L, et al. Study of synthesis and corrosion inhibition of novel mannich and schiff bases on carbon steel in acid solution. Russ J Appl Chem. 2018;91(3):499–509.
- 22. Quraishi MA, et al. N-(Piperidinomethyl)-3-[(pyridylidene)amino]isatin: A new and effective acid corrosion inhibitor for mild steel. Mater Chem Phys. 2008;112(3):1035–9.
- 23. Umoren SA, et al. Inhibition of mild steel corrosion in HCl solution using chitosan. Cellulose. 2013;20(5):2529–45.
- 24. Tai ZX, Fei YY, Min QC. Study on Aromatic Ketone Manichbase Series Acidification Inhibitors. Materials Protection. 2007;40012:60–6.
- Arend M, Westermann B, Risch N. Modern Variants of the Mannich Reaction. Angewandte Chemie Int. 1998;378:1044–70.
- 26. El-masry X, et al. Synthesis and Antimicrobial Activity of Some New Benzimidazole Derivatives. Molecules. 2000;9:89.
- 27. Yu L. Some consideration on the Langmuir isotherm equation. Colloids Surf, A. 2006;274(1–3):34–6.
- 28. Jagieo J, Schwarz JA. Local exact and approximate solutions of the adsorption integral equation with a kernel of a Langmuir-like isotherm: determination of adsorption energy distribution. J Colloid Interface Sci. 1991;146(2):415–24.
- Cano E, et al. A study on the adsorption of benzotriazole on copper in hydrochloric acid using the inflection point of the isotherm. Adsorp J Int Adsorp Soc. 2004;10(3):219–25.
- 30. Larabi L, et al. 2-Mercapto-1-methylimidazole as corrosion inhibitor for copper in hydrochloric acid. Appl Surf Sci. 2006;253(3):1371–8.
- Blg S, AlSkan N. Effect of N-(1-toluidine) salicylaldimine on the corrosion of austenitic chromium-nickel steel. Appl Surf Sci. 1999;152(1–2):107–14.

### **Publisher's Note**

Springer Nature remains neutral with regard to jurisdictional claims in published maps and institutional affiliations.